



*Tunable and efficient catalysts for the simultaneous trans-esterification of lipids and esterification of free fatty acids from bio-oils for an effective production of FAMES*

EuroBioRef Summer School,  
September 18<sup>th</sup>-24<sup>th</sup>, 2011, Lecce, Italy

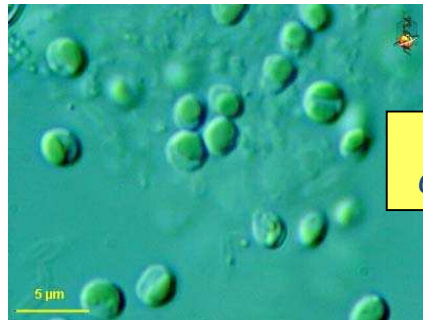


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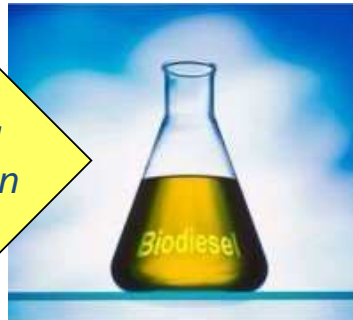
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# Introduction

## Utilization of aquatic biomass

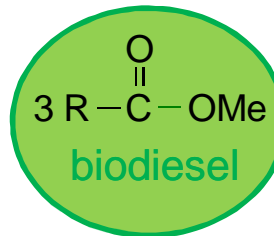
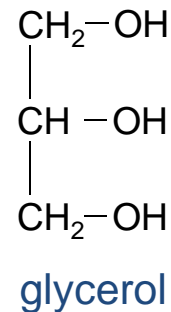
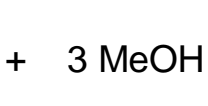
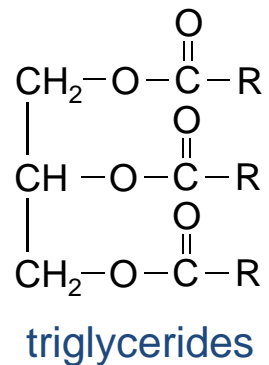


chemical conversion



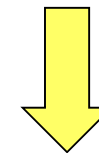
### Disadvantages

- may contain up to 20% of free fatty acids-FFAs
- it is formed by a mixture of poly-unsaturated fatty acids-PuFAs



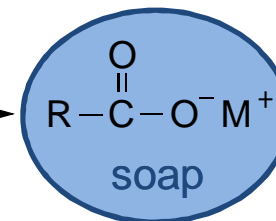
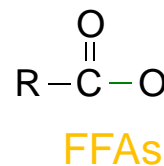
### Basic catalysts

NaOH, KOH, carbonate or alkoxides



FFAs exceed 0.1-0.5 %wt

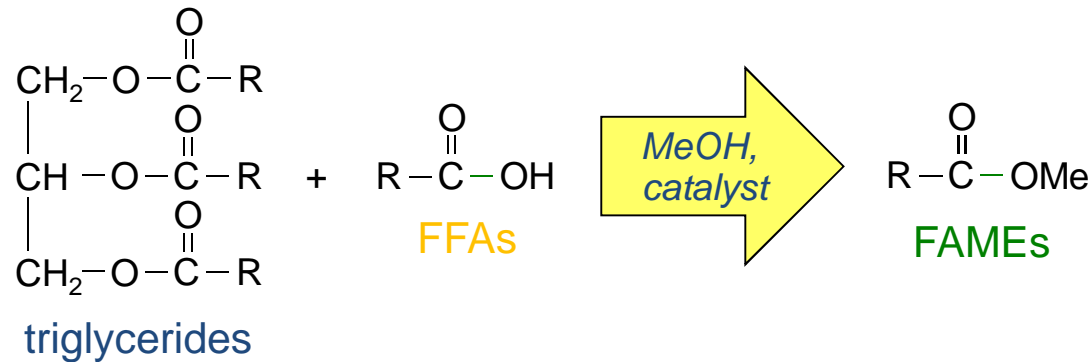
- formation of gels
- increase of viscosity
- high cost of separation



M = Na, K

# Scope of study

Our approach to the treatment of **bio-oil** is based on the use of **solid bifunctional catalysts** that are able to catalyze the simultaneous trans-esterification of lipids and esterification of **FFAs**



## Catalysts

- ◆  $\text{CaCO}_3$
- ◆  $\text{Al}_2\text{O}_3$
- ◆  $\text{CeO}_2$
- ◆  $\text{xCaO} \cdot \text{yAl}_2\text{O}_3$
- ◆  $\text{xCaO} \cdot \text{zCeO}_2$
- ◆  $\text{yAl}_2\text{O}_3 \cdot \text{zCeO}_2$
- ◆  $\text{xCaO} \cdot \text{yAl}_2\text{O}_3 \cdot \text{zCeO}_2$

## Preparation method: solid state synthesis

- 🌱 **Reagents:**  $\text{Ce}(\text{NO}_3)_3 \cdot 6 \text{H}_2\text{O}$ ,  $\text{CaCO}_3$  and  $\gamma\text{-Al}_2\text{O}_3$
- 🌱 Anidrification
- 🌱 Mixing and homogenization in a High Energy Milling HEM apparatus for 1 h at a speed of 700 rpm
- 🌱 **Calcination for 3 h at 823 and 1373 K**

## Characterization

- Elemental analysis
- DRIFT
- BET Surface Area
- Acid and basic sites

# Catalytic tests 1

*New mixed oxides* based on calcium, cerium and aluminium have been used as catalysts in the reaction of trans-esterification of *extra-virgin oil* as test case

## Extra-virgin oil

**Table 1.** Trans-esterification of extra-virgin oil using several mixed oxides (Bold characters evidentiate biodiesel responding to EU regulations)

Catalyst	% Composition organic phase				Saponifiable matter
	FAMEs	MG	DG	TG	
Oil used	0	1.07	2.71	93.45	97.23
CaCO <sub>3</sub>	7.6	1.55	8.20	72.37	89.72
Al <sub>2</sub> O <sub>3</sub>	15.1	3.69	8.66	62.93	90.38
CeO <sub>2</sub>	11.1	0.90	6.00	75.63	93.63
<b>CaO·CeO<sub>2</sub></b>	<b>97.0</b>	<b>0.79</b>	<b>0.07</b>	<b>0.11</b>	<b>97.97</b>
12CaO·7Al <sub>2</sub> O <sub>3</sub>	50.4	11.16	8.75	20.17	90.48
12CeO <sub>2</sub> ·7Al <sub>2</sub> O <sub>3</sub>	5.7	0.31	3.71	84.56	94.28
<b>12CaO·7Al<sub>2</sub>O<sub>3</sub>·3 CeO<sub>2</sub></b>	<b>96.8</b>	<b>0.80</b>	<b>0.02</b>	<b>0.05</b>	<b>97.67</b>
<b>12CaO·7Al<sub>2</sub>O<sub>3</sub>·7 CeO<sub>2</sub></b>	<b>96.7</b>	<b>0.65</b>	<b>0.01</b>	<b>0.01</b>	<b>97.37</b>
<b>12CaO·7Al<sub>2</sub>O<sub>3</sub>·12 CeO<sub>2</sub></b>	<b>96.1</b>	<b>0.80</b>	<b>0.01</b>	<b>0.01</b>	<b>97.92</b>

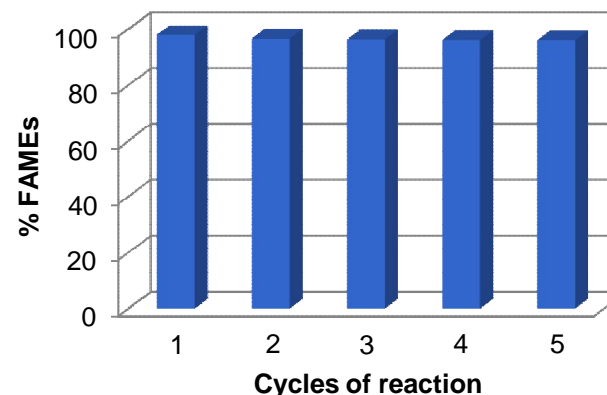
M. Aresta, A. Dibenedetto, M. Ricci ENI patent H10008, 2010

## Trans-esterification tests

- ◆ **Reagents** - 1.8 g of starting oil  
- 0.05 g of catalyst  
- 5 mL of methanol
- ◆ **Pressure** 5 MPa of N<sub>2</sub>
- ◆ **Temperature** 453 K for 3 h

The catalysts calcinated at 823 K show the best catalytic activity in trans-esterification process: with **12CaO·7Al<sub>2</sub>O<sub>3</sub>·7CeO<sub>2</sub>** shows a very good stability without any loss of activity over 5 cycles

**Figure 1.** Recycling test of 12CaO·7Al<sub>2</sub>O<sub>3</sub>·7CeO<sub>2</sub>



# Catalytic tests 2

## Lampante olive oil

Ceria alone has good catalytic properties for the direct esterification of FFAs into methyl-esters

Mixed oxides composed by calcium and ceria show a good activity in both the trans-esterification of TG and direct esterification of FFAs, aluminium does not improve the catalytic activity but increases the stability of catalyst

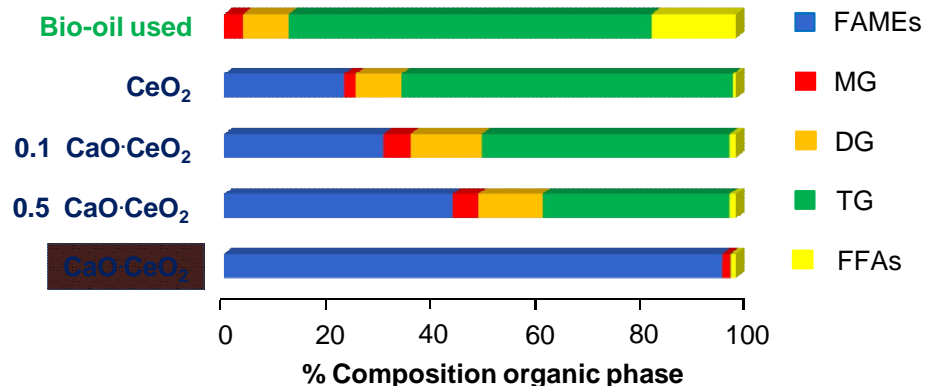
**Table 2.** Reactivity of mixed oxides in the trans-esterification of lampante olive oil.

Catalyst	% Composition organic phase					Saponifiable matter
	FAMEs	MG	DG	TG	FFA	
Oil used	0	1.24	5.83	72.92	18.68	98.67
CaCO <sub>3</sub>	17.92	3.85	13.52	47.17	14.57	97.03
Al <sub>2</sub> O <sub>3</sub>	13.22	2.61	11.96	54.88	15.70	98.37
CeO <sub>2</sub>	26.49	0.55	7.67	63.23	0.32	98.26
<b>CaO·CeO<sub>2</sub></b>	<b>95.62</b>	<b>0.91</b>	<b>0.02</b>	<b>0</b>	<b>0.68</b>	<b>97.23</b>
CaO·Al <sub>2</sub> O <sub>3</sub>	28.57	5.85	13.98	35.97	13.45	97.82
<b>12CaO·7Al<sub>2</sub>O<sub>3</sub>·7CeO<sub>2</sub></b>	<b>95.48</b>	<b>0.88</b>	<b>0.01</b>	<b>0.01</b>	<b>0.70</b>	<b>97.08</b>

## Bio-oil extracted from microalgae

The catalytic activity of mixed oxides Ca/Ce is connected to the calcium content correlated to the increase of acid and basic sites

**Figure 2.** Trans-esterification of bio-oil extracted from microalgae (Operative conditions: 1h at 353 K, MeOH/oil = 150:1)



### Biodiesel composition

FAMEs > 96%

Residual content of FFAs < 0.5%

# Conclusion

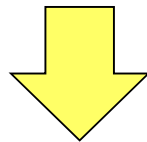
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In this work, new mixed oxides have been used as catalysts in the conversion of bio-oil with different lipids-FFA composition

extra-virgin oil

lampante olive oil

oil extracted from aquatic biomass



$\text{CaO}\cdot\text{CeO}_2$  and  $12\text{CaO}\cdot 7\text{Al}_2\text{O}_3\cdot 7\text{CeO}_2$  show the best catalytic activity in both the trans-esterification of lipids and esterification of FFAs with the resulting biodiesel being well within the EU specifications

A. Dibenedetto, C. Pastore, L. di Bitonto, A. Colucci and M. Aresta,  
***“Bifunctional catalysts: tunable and efficient agents for the simultaneous trans-esterification of lipids and esterification of free fatty acids from bio-oils”***, submitted

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